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to another unit. If the process °uid is not at the desired setpoint temperature, the performance of the unit (reactor, etc) may not be as good as desired, and therefore not as profitable. i. The control block diagram for the process furnace is shown below in Figure 1. Where the the signals as Figure 1-1: Control block diagram of process ...

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Chapter 8 Solutions 8.1
Missing 8.2 From the
block diagram $y(s) =$
 $g_p(s)u(s) + g_d(s)l(s)$
and $u(s) = q(s)r(s) -$
 $\tilde{d}(s)$ but $\tilde{d}(s) = y(s) -$
 $\tilde{y}(s)$ $\tilde{y}(s) = \tilde{g}_p(s)u(s)$
then $\tilde{d}(s) = y(s) -$

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$$\tilde{g}_p(s)u(s) \text{ and } u(s) = \frac{1}{q(s)}[r(s) - y(s)]$$

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Step-by-step solution:

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Step 1 of 5 (a) There are three important process variables in a process control system. Feedback control system measures the controlled variable and compares the measured value with the desired value and then adjusts the manipulated variables for the control of the system accordingly.

Process Dynamics

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8.2 The tank system operates at steady state. At $t = 0$, 10 ft^3 of water is added to tank 1. Determine the maximum deviation in level in both tanks from the ultimate steady state values, and the time at which

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each maximum occurs.
 $A_1 = A_2 = 10 \text{ ft.}$ $R_1 = 0.1 \text{ ft/cfm}$
 $R_2 = 0.35 \text{ ft/cfm.}$

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objectives can be
formulated for practice,
the term process tends
to be used for both
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distillate the processing operation and the processing composition can be controlled by adjusting the equipment. reflux flow rate or the distillate flow rate.

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Step 2 of 4 The tank system is provided with two streams, the steam 1 and steam 2. The outlet for steam 3 reduces the excess steam in the tank. Write the mass balance equation for the overall tank system. The mass of material is, Substitute for m in the mass balance equation.

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